

Alternatives to Electricity for GW-scale Transmission and Firming Storage for Diverse, Stranded Renewables: Hydrogen and Ammonia

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Abstract— We must soon “run the world on renewables” but cannot, and should not try to, accomplish this entirely with electricity transmission. The world’s richest renewable energy (RE) resources – of large geographic extent and high intensity – are stranded: far from end-users with inadequate or nonexistent gathering and transmission systems to deliver the energy. Electricity energy storage cannot affordably firm large, intermittent renewables at annual scale, while gaseous hydrogen (GH2) and anhydrous ammonia (NH₃) fuels can: GH2 in large solution-mined salt caverns, NH₃ in surface tanks.

At GW scale, renewable-source electricity from diverse sources can be converted to hydrogen and byproduct oxygen, and/or to NH₃, pipelined underground to load centers for use as vehicle fuel and combined-heat-and-power generation on the wholesale or retail side of the customers’ meters. The ICE, CT, and fuel cell operate very efficiently on GH2 and NH₃ fuels. USA has extensive extant NH₃ pipeline and tank storage infrastructure.

Index Terms — Ammonia, cavern, firm, fuel, packing, pipeline, renewable, storage, stranded, tank, transmission

I. INTRODUCTION

HUMANITY must quickly convert our global energy system from fossil to primarily renewable energy (RE) sources. We will need more transmission and storage capacity than electricity can provide. Thus, we need to now investigate and plan for a diversity of complementary RE transmission and storage media, fuels, systems, and strategies; gaseous hydrogen (GH2) and anhydrous ammonia (NH₃) are especially attractive; transmission pipelines for both have multi-GW capacity over hundreds of km. Our investigation must embrace complete RE systems, as envisioned by Ocean Energy Institute in Fig. 7.

The energy output of most renewables varies greatly, at time scales of seconds to seasons: the energy capture assets thus operate at inherently low capacity factor (CF); energy delivery to end-users is not “firm”. New electric transmission systems, or fractions thereof, dedicated to renewables, will suffer the same low CF, and represent substantial stranded capital assets, which increases the cost of delivered renewable-source energy. We cannot achieve California AB32 and other

ambitious greenhouse gas (GHG) emissions goals without fuel cell vehicles (FCV’s) fueled with large quantities of zero-carbon-source GH2 fuel. GH2 pipelines may have a major role in humanity’s energy future. Large-scale gathering, transmission, and distribution of RE-source GH2 fuel in pipelines would be a major new industrial process, for which a pilot plant is required, on the critical path to discovering and demonstrating feasibility. No GH2 pipelines for renewables-hydrogen service exist; the extensive extant industrial GH2 pipeline system is not capable of renewables-hydrogen service, over hundreds of km with large and frequent pressure fluctuation.

We report the results of several studies of the technical and economic feasibility of large-scale RE – hydrogen systems. [1-6, 20] NH₃ is also an attractive transmission and storage medium, and strategy. Pressurized NH₃ storage and delivery infrastructure is very similar in design and performance to propane (LPG). The ICE, CT, and direct ammonia fuel cell operate very efficiently on NH₃ fuel. Energy, as liquid ammonia fuel, is stored inexpensively in 10-30,000 ton refrigerated surface tanks. Extensive pipeline and tank infrastructure is in place in USA. Since ammonia can be shipped and stored in mild steel pipelines and tanks, any natural gas or petroleum pipeline could be easily converted to carry NH₃.

Underground transmission pipelines, as would be required for GH2 and NH₃, are typically easier to site and permit than electric lines, and each may have multi-GW capacity.

Relieving RE generation / conversion equipment of the requirement to deliver “grid quality” AC (V, f, PF, and harmonics) as well as “low voltage ride through” (LVRT), because RE electricity is entirely delivered to electrolyzers and NH₃ synthesis systems, may significantly reduce the capital and O&M costs of RE.

The wind energy of the twelve Great Plains states, if fully harvested on about 50% of these states’ aggregate land area, transmitted to distant markets, and “firmed” at annual scale with energy storage, could supply the entire annual energy demand of the USA: about 10,000 terawatt-hours (TWh = billion kWh), or about 100 quads (quadrillion btu). [12] However, existing Great Plains electric transmission export capacity is insignificant relative to this resource. Any large,

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new electric transmission systems, or fractions thereof dedicated to wind energy, will:

- Be very costly to build;
- Be difficult to site because FERC has no authority for permitting interstate electric lines;
- Be difficult to site and permit, because of public objection, as in NIMBY;
- Suffer the same low capacity factor (CF) (typically 40%) as the windplants and other RE plants they serve, unless RE generation is curtailed;
- Provide no affordable “firming” (weekly-to-annual scale) energy storage, thus taxing the “system balancing” ability of the electricity grid;
- Be vulnerable to damage by acts of God and man.

Two transmission and annual-scale, firming storage schemes seem technically and economically attractive for wind and other time-varying-output renewable electric energy sources at GW (nameplate) scale:

1. Conversion of electric energy to GH₂, by electrolysis of water, at high pressure (30 – 150 bar); GH₂ transmission and delivery by underground pipeline, with annual-scale firming storage of high-pressure GH₂ in deep, solution-mined salt caverns;
2. Conversion of electric energy to NH₃, for transmission as liquid by underground pipeline, delivery via pipeline, rail, and truck, with annual-scale firming storage as liquid NH₃ in large (10,000 – 60,000 ton) refrigerated, above-ground tanks.

Without any expansion of electricity transmission capacity, or technology breakthroughs, RE may be totally converted to GH₂ or NH₃, transmitted over long distances using new or repurposed underground pipelines, firmed at annual scale in large GH₂ storage caverns and above-ground NH₃ tanks, and marketed as fuel for vehicles and for combined-heat-and-power (CHP) distributed generation in:

- Internal combustion engine (ICE) and combustion turbine (CT) gensets adapted for NH₃ fuel;
- PEM hydrogen fuel cells, for GH₂ and hydrogen “cracked” from NH₃;
- Direct-ammonia fuel cells.

The ICE operates efficiently on either GH₂ or NH₃ fuel, and is a mature technology for both.

Total installed capital cost of large, underground NG pipelines is now \$US 50-60 per inch diameter per meter length, without compression, which adds ~ 15% to pipeline capital cost [14, 15]. Pipeline costs vary considerably, among projects, and with material prices and contractor availability. We assume that NH₃ pipelines, and GH₂ pipelines fit for renewables-hydrogen service, can be built for the same cost as NG pipelines of the same diameter and rated pressure, assuming no incremental capital costs for GH₂-capable line pipe, valves, and meters.

GW-km is a measure of the total transmission service provided by the system, useful for comparing transmission

means and strategies. Large electric transmission lines cost about \$1 million per GW-km as Frontier Line components [13].

Fig. 1 shows the capacity of a 36” GH₂ pipeline 800 km long is ~ 8 GW; thus total system capacity is 6,400 GW-km. From the estimate above, pipeline capital cost is ~ \$US 1.4 billion, assuming no GH₂ compression. Then, cost per GW-km is ~\$240,000

A 10” mild steel pipeline, 1,000 km long, for liquid NH₃ at ~20 bar, has a continuous capacity of ~1 GW [17], with adequate pumping at midline stations, which would be adequate for a 2.5 GW nameplate windplant with internal NH₃ output smoothing or firming storage. Pipeline total installed capital cost is ~\$600,000 per km, including pumping stations. A 1,000 km pipeline would cost ~\$US 600 million; total system capacity is 1,000 GW-km; cost per GW-km is ~\$600,000

Thus, the relative capital cost of transmission systems may be approximately compared, per GW-km:

Electricity, 500 kV, AC or DC	\$ 1 million
GH ₂ pipeline, no compression	\$ 240K
Liquid NH ₃ pipeline, with pumping	\$ 600K

New underground pipelines are generally less controversial, thus faster and easier to site and permit, than new overhead electric transmission lines. Pipelines are generally better protected from acts of God and man.

II. TECHNICAL WORK PREPARATION

We estimate costs of transmission and annual-scale firming storage of diverse, GW-scale, stranded renewables. No pilot plant exists for confirming the system capital costs and conversion efficiencies we estimate in this study, although both GH₂ and NH₃ have been proposed for wind energy transmission and storage [1-6, 20]. Hydrogen is promising as a clean-burning energy carrier, and modern electrolyzers can produce large volumes of high-pressure hydrogen, ready for direct pipeline transmission and/or for ammonia synthesis, from renewable energy sources. Renewable-source hydrogen can alternatively be stored and transported as NH₃, which can be readily synthesized, following electrolysis, using atmospheric nitrogen, and be used at the delivery end-point as a fertilizer or a fuel. Both GH₂ and NH₃ transmission and firming storage will accelerate our conversion from fossil to diverse renewable resources, via major new markets including, and beyond, the electricity sector.

A. Electricity Transmission and Storage

Making the electricity grid “smart” will add some virtual transmission capacity but no physical capacity. The marginal cost of grid integration for wind, and other renewables, will increase with the fraction of total energy supplied by renewables (except geothermal), in spite of valiant technical and policy integration efforts. [7]

Several hundred GW of new electricity transmission for RE, as proposed in Frontier Line, Green Power Express, Trans West Express, and others:

- In aggregate capacity accommodate only a small fraction of the RE needed to meet climate change mitigation goals;
- May be blocked, for too long, by local jurisdictions and popular opposition;
- Cannot presently benefit from FERC, which lacks interstate jurisdiction for electricity line right-of-way and permitting.

Our electricity transmission cost benchmark is the Frontier Line Feasibility Study, which considered many multi-GW electricity transmission expansions, all at 500 kV, both AC and DC, from Wyoming south and west, with these typical results [13, 18]:

- AC line construction cost \$ 29.90 / MWh
- DC line construction cost \$ 19.10 / MWh
- California system integration \$ 3.00 / MWh
- Line losses \$ 1.80 / MWh

Analysis of individual Frontier Line transmission links gives these mean capital costs for mixed AC and DC lines:

- Per GW \$ 619 million
- Per mile \$ 4.9 million
- Per GW-mile \$ 1.4 million
- Per GW-km \$ 0.9 million

Analysis of complete Frontier Line transmission system alternatives gives these mean capital costs:

- Per GW \$ 1,375 million
- Per mile \$ 3.2 million
- Per GW-mile \$ 0.8 million
- Per GW-km \$ 0.5 million

GW-mile and GW-km are measures of the total transmission service provided by the system. Whether these Frontier Line estimates include ROW lease or purchase is unknown. Large electric transmission lines cost \$500K – \$900K per GW-km.

B. GH₂ Transmission and Storage

GH₂ transmission requires line pipe material and system components able to resist and control, or be immune to, hydrogen embrittlement (HE). In contrast, NH₃ pipelines are moderate-strength, low-alloy, carbon steel. NH₃ does not attack steel.

Fig. 2 shows one solution to the HE danger, whereby the structural strength of steel is replaced by fiber-reinforced plastic (FRP) and the GH₂ permeation barrier is reduced to a thin Cu or Al foil.

Fig. 3. Without any expansion of the electricity transmission grid, all RE is converted at the windplant or other RE plant to GH₂ fuel. High-pressure-output electrolyzers feed the pipeline directly at ~100 bar, from wind or other RE electricity sources. Other RE-source GH₂ is delivered to the pipeline via compressors. Wind and other RE generators are interconnected via pipelines rather than via field-voltage electricity collection cables. The oxygen byproduct of

electrolysis may be sold to adjacent coal and dry biomass gasification plants. A small amount of distribution-level electricity is required for the RE generation control systems.

Fig. 4. GH₂ is stored at 100-150 bar in solution-mined salt caverns, typically 800,000 cubic meters physical volume, capable of storing ~ 2,500 net tons of GH₂ in addition to ~2,000 tons of “cushion” GH₂. The cavern top is typically ~800 m below ground level. The surface facility provides compression (if needed), GH₂ gas drying upon withdrawal, and manifolding of multiple caverns in a storage array. Typically, capital cost of a completed facility is half cavern excavation, half surface facility. In Texas onshore domal salt, in a multi-cavern facility achieving maximum economy of scale, each cavern will cost ~\$15-20 million and will store ~2,500 net tons GH₂. Leakage and O&M cost, except for compression energy (if required), are very low.

About 15,000 such salt caverns could firm, at annual scale, the entire Great Plains, USA, wind resource, as GH₂ fuel: ~10,000 TWh (~100 quads) per year. Synergy with solar and other renewables would reduce required cavern storage, perhaps dramatically. However, customers must now purchase energy only as GH₂ fuel.

Germany considers GH₂ cavern storage more attractive than compressed air energy storage (CAES) for integrating wind on their electricity grid. [9]

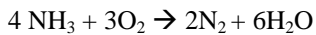
C. NH₃ Transmission and Storage

Iowa State University has hosted six annual Ammonia Fuel Conferences, which include NH₃ as an RE transmission and storage medium, as well as a transportation and distributed generation fuel. [10]

NH₃ contains no carbon; has physical properties similar to propane; liquefies at ambient temperatures at about 10 bar or at -33 degrees C at 1 atmosphere. Liquid ammonia has over 50% more volumetric energy than liquid hydrogen; more than twice the volumetric energy of hydrogen gas at 700 bar. It is the second-largest-volume industrial chemical in global trade: ~130 MMT / year, mostly for N-fertilizer. USA consumes ~15 MMT / year, with a good safety record. NH₃ is classified as an “inhalation hazard”.

NH₃ is nearly 18% hydrogen by weight and has slightly over half the energy density of gasoline by volume. All of ammonia’s energy is derived from its hydrogen content; it can be easily reformed to hydrogen and nitrogen, with N₂ returned to its source, Earth’s atmosphere. NH₃ has the highest hydrogen content by volume of any liquid fuel, including gasoline, liquefied natural gas (LNG), liquefied petroleum gas (LPG, propane), ethanol, and even liquid hydrogen. Liquid anhydrous ammonia, NH₃, has more atoms of hydrogen per liter than liquid hydrogen. This ability of NH₃ to store hydrogen very compactly at ambient temperature and moderate pressure is a key advantage for NH₃ over GH₂.

Like hydrogen, ammonia can burn directly in spark-ignited internal combustion engines and may also be fed directly to medium temperature solid oxide, proton-conducting ceramic, and molten-salt direct-ammonia fuel cells. Ammonia combusts according to:



with only nitrogen and water vapor as combustion products. Like hydrogen, ammonia is lighter than air and is not a greenhouse gas.

Figs. 5 and 6 show NH_3 value as an alternative to electricity for GW-scale RE transmission and storage. However, the electrolysis-plus-H-B synthesis process shown in Fig. 6 has too much capital cost operating at low CF, with the estimated cost of wind-source NH_3 at the plant gate $> \$1,000 / \text{MT}$, which is not competitive with domestic or imported fossil-source NH_3 . Consequently, SSAS, shown in Fig. 8, was developed to reduce the cost of RE-source NH_3 . However, SSAS has not yet been demonstrated at commercial scale.

Fig. 9 shows that a safe, reliable, proven ammonia delivery and storage infrastructure already exists in the US. Approximately 3,000 miles of carbon-steel ammonia pipeline is in service in America's agricultural heartland, mainly in the Corn Belt. Almost a hundred large terminals for refrigerated ammonia storage are distributed along the pipeline. Barges, trains, and trucks round out the delivery system, which supplies the ammonia from the terminal to the farmer when he needs it for the growing season. The state of Iowa, alone, has over 800 retail outlets where farmers buy "anhydrous" or "nitrogen", the vernacular for ammonia fertilizer, NH_3 .

About 20,000 MW of nameplate Great Plains wind generation would be needed to produce 6 million tons of NH_3 per year, about one-third of the present USA demand for ammonia based fertilizer [21]. This estimate is based on an overall 50% efficiency of converting wind power into energy stored as NH_3 . Several times as much wind, or other renewables generation, would be needed to produce all of the USA NH_3 demand, especially if NH_3 also becomes widely adopted as a fuel.

A large, liquid ammonia "atmospheric" storage tank typical in the Corn Belt, USA, stores refrigerated NH_3 at 1 atm, -33C . Typical capacity is 30,000 MT, equal to 190 GWh as H_2 reformed from NH_3 . This size mild steel, double-wall tank would cost $\sim \$15\text{M}$, or $\sim \$77 / \text{MWh}$.

D. Energy Storage Required to "Firm" Great Plains Wind

The modern world requires "firm" energy, which must mean that, every hour of every year:

- A supplier and buyer can contract for an agreed amount of energy;
- Energy demand, as managed and as variable, is met.

Consider the quantity of GH2 storage required to "firm" the output of a 2,000 MW (nameplate) Great Plains windplant which produces $\sim 7 \text{ TWh}$ in an average year. Using the numbers from "Seasonal Variability of Wind Electric Potential in the United States" [19], Table 3, for "North Central", normalized, yields these "seasonality factors":

Winter 1.20 Spring 1.17 Summer 0.69 Autumn 0.93

We find that expected average seasonal energy production for the 4,000 MW windplant would be $(7 \text{ TWh} / 4 \text{ seasons}) = (1.75 \text{ TWh}) \times \text{seasonality factor}$, above:

Winter = $1.75 \times 1.20 = 2.10 \text{ TWh}$
 Spring = $1.75 \times 1.17 = 2.05 \text{ TWh}$
 Summer = $1.75 \times 0.69 = 1.21 \text{ TWh}$
 Autumn = $1.75 \times 0.93 = 1.63 \text{ TWh}$

The biggest difference between seasons is between Winter and Summer: $2.10 - 1.21 = 0.89 \text{ TWh}$. If all windplant energy is converted to GH2 for export, at the 75% efficiency typical of large-scale electrolyzers, this is apparently 0.71 TWh of GH2 storage needed. However, the biggest difference between adjacent, sequential seasons is between Spring and Summer: $2.05 - 1.21 = 0.84 \text{ TWh}$. If all windplant energy is converted to GH2 for export, at 75% electrolyzer efficiency, apparently $[0.84 \times 0.75 = 0.63] \text{ TWh} = 630 \text{ GWh}$ of GH2 storage is needed. The latter case is more relevant. Stored as "electricity" at 100% round-trip ideal efficiency, without 25% energy conversion loss in electrolysis, $\sim 470 \text{ GWh}$ storage would be needed.

GH2 transmission pipelines are likely to operate at 100 – 150 bar maximum input pressure, with city-gate delivery at ~ 30 bar. An 800 km, 20" diameter GH2 pipeline, packed to 130 bar and unpacked to 65 bar, stores 936 tons of GH2 = 33,500 MWh. = 0.03 TWh, which we assume for this analysis.

Thus, geologic storage needed to seasonally "firm" 2,000 MW (nameplate) of Great Plains wind, over the maximum average seasonal variation, is: $0.63 - 0.03 = 0.6 \text{ TWh}$, which is equivalent to $\sim 18,000$ metric tons (MT) of GH2.

Thus, annual-scale firming of the output of a 2,000 MW (nameplate) windplant in the northern Great Plains requires energy storage of approximately:

- 450,000 MWh as electric energy, for which no affordable mechanism exists, or
- 18,000 tons of GH2, requiring about 6 large, solution-mined salt caverns [6], or
- 110,000 tons of NH_3 , requiring about 4 typical, large, refrigerated, above-ground tanks.

No affordable electric energy storage technique or system capable of 470,000 MWh, for annual-scale firming of this quantity of Great Plains wind, is available or anticipated. The vanadium-redox battery energy storage system (VRB-ESS) presently provides the lowest-cost bulk electricity storage. VRB Power Systems, Canada, will sell a VRB-ESS flow battery to Tapbury Management, County Donegal, Ireland, for $\$US 6.3$ million: 1.5 MW (charge and discharge rate), 12

MWh (total energy storage capacity) [18]. Storing 450,000 MWh would require ~37,000 of this VRB-ESS, at total capital cost > \$US 100 billion, if mass production halved VRB-ESS cost and if the optimum power: energy ratio for VRB-ESS components were determined.

Compressed air energy storage (CAES) may provide lower-cost “electricity” storage, but we need as-built storage capacity and capital and O&M costs for the proposed Iowa Stored Energy Park. [14] No CAES plants have been built for decades, so costs are uncertain. Continental CAES capacity may be too geologically limited to facilitate the very large scale RE supply of firm energy humanity needs.

USA has several salt deposit realms with formations deep and tight enough to store GH₂ in man-made caverns at 150 bar with negligible leakage. Fig. 4 shows GH₂ storage caverns. Total capital cost for the 6 required GH₂ caverns would be about \$95M; for the 4 required NH₃ tanks would be about \$90M. The wind or other RE is now sold as GH₂ or NH₃ fuels for vehicles and DG of electricity in stationary CHP.

The oxygen byproduct of water electrolysis may be sold to adjacent new dry biomass and / or coal gasification plants, likely to be prevalent in the Great Plains.

Consider the optimistic estimated cost of annual firming storage for wind-source NH₃ production in a complete SSAS system with a 1,600 km NH₃ transmission pipeline: Fig. 8.

Total Installed Capital Cost	
1,600 km pipeline with “Firming” NH ₃ tank storage:	
Windplant size	1,000 MW
Wind generators	\$ 1,000 [million]
ASU	100
SSAS Reactors	500
Pipeline, 10”	500
(2) NH ₃ storage tanks @ \$15M ea	30
TOTAL	\$ 2,130
Tank storage: ~ 1 % of total capital cost	

E. Storage Cost Comparison

Delivering annually-firm energy from Great Plains wind will require ~ 300,000 GWh of storage per 1,000 MW of nameplate wind capacity. At this seasonal scale, power (charge and discharge rate) rating is much less important than energy rating. Estimated capital costs of 300,000 GWh storage:

As “electricity” in Vanadium Redox Battery (VRB)	\$100B
As GH ₂ in salt caverns	\$100M
As NH ₃ in “atmospheric” surface tanks	\$ 90M

Relatively little energy is required to compress GH₂ to ~ 150 bar for optimal salt cavern economic utilization, and to dry the GH₂ upon withdrawal from the cavern.

Relatively little energy is required to refrigerate the large (10-30,000 MT) “atmospheric” NH₃ storage tanks and to pump the pressurized liquid NH₃ upon withdrawal from the tank.

Arraying caverns and tanks to increase total storage capacity while sharing balance-of-plant infrastructure would further reduce energy capacity capital and O&M costs.

F. Pilot Plants Needed

We should assemble consortia to begin immediately to design and build pilot plants for RE-source GH₂ and NH₃ transmission and firming storage, by which to discover and demonstrate their technical and economic feasibility – or lack thereof:

- Conceive: perform technical and economic feasibility studies; describe needed upstream R&D;
- Design: propose preliminary design specifications;
- Design: release a credible RFP or RFQ to determine costs to design, build, and operate the pilot plants;
- Build, own, operate: assemble a collaborative to fund the projects, to supply renewable-source GH₂ and NH₃ fuels to the pilot plants, and to use the delivered fuels.

This pilot plant concept has been proposed as the International Renewable Hydrogen Transmission Demonstration Facility (IRHTDF). [2]

G. Further Work Needed

1. Develop new technologies and components for higher energy conversion and synthesis efficiency at lower capital and O&M costs. Continuous improvement via R&D and demonstrations.

2. Fig. 8. Solid state ammonia synthesis (SSAS), now a patented laboratory-scale device, needs R&D and demonstration at ~100 kW synthesis module scale, to learn whether it offers an economically-superior path to RE-source NH₃ production, vis-à-vis the Haber-Bosch synthesis path.

3. Model continental-scale, multi-GW RE systems, to suggest optimum mix of electricity, GH₂, NH₃, and perhaps other transmission and firming storage strategies.

H. Conclusion

Only expanding, and making “smarter”, the electricity gathering-transmission-storage-distribution grid will not allow replacing fossil-source energy with RE-source energy quickly enough to meet humanity’s goal of preventing rapid and catastrophic climate change, by quickly reducing GHG emissions.

We will need other transmission and storage media, systems, and strategies in addition to electricity. GH₂ and NH₃ are attractive alternatives, for which pilot plants should soon be built, in order to discover and demonstrate their technical and

economic feasibility and their acceptability to the public and to the business and finance communities. Both GH₂ and NH₃ provide affordable seasonal-to-annual-scale firming storage for diverse RE resources, as well as the transmission paths for bringing GW-scale, stranded RE to distant markets. End-users purchase their energy as GH₂ and / or NH₃ fuels, for CHP on-site generation, centralized generation, and for transportation fuels and for space-conditioning and industrial uses. Transmission pipelines for both GH₂ and NH₃ fuels have multi-GW capacity over hundreds of km.

III. ACKNOWLEDGMENT

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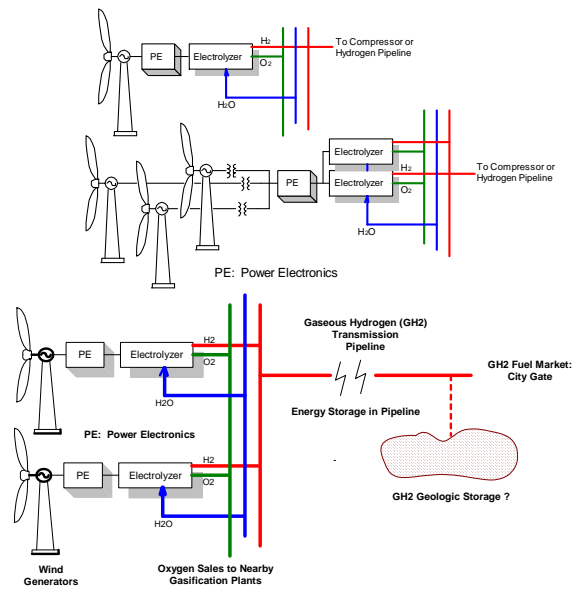


Fig. 3. System topology options for wind-to-hydrogen energy conversion, gathering, and transmission. The hydrogen may be delivered to transmission pipelines or to nearby NH₃ synthesis plants. Both GH₂ and NH₃ may be stored for affordably firming wind and other RE.

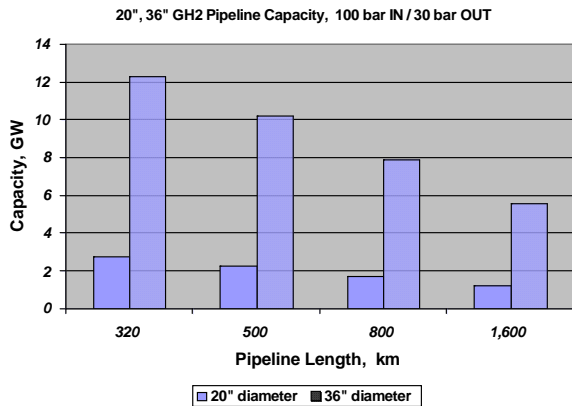


Fig. 1. Capacity of GH₂ transmission pipelines, assuming: no input or midline compression; high-pressure-output electrolyzers deliver directly to pipeline at 100 bar; pipeline friction losses are accepted; delivery to city-gate market at 30 bar. Total transmission service capacity of an 800 km, 36" pipeline is ~6,400 GW-km.

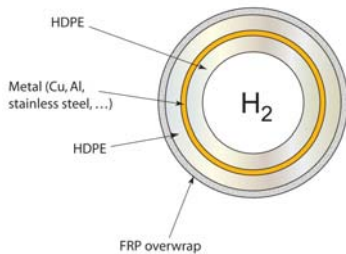


Fig. 2. Hydrogen Discoveries, Inc. (HDI) Polymer/Metal Pipe Technology, which avoids hydrogen embrittlement (HE, HCC) by eliminating alloy steel as a structural material. Primary GH₂ diffusion barrier is a thin metal foil. This pipe can be fabricated up to 1m diameter, in the field, in unlimited lengths.

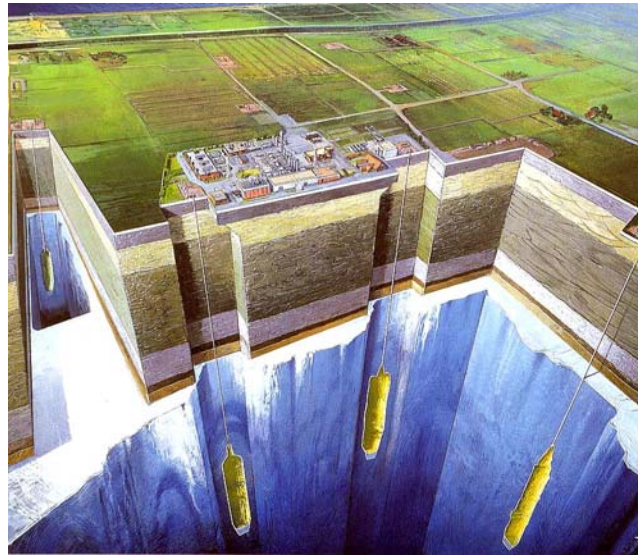


Fig. 4. Multiple large, solution-mined salt caverns in "domal" salt, suitable for high-pressure storage of GH₂. A typical cavern will store 2,500 net Mt of GH₂ at 70-150 bar in ~800,000 cubic meters of physical volume.

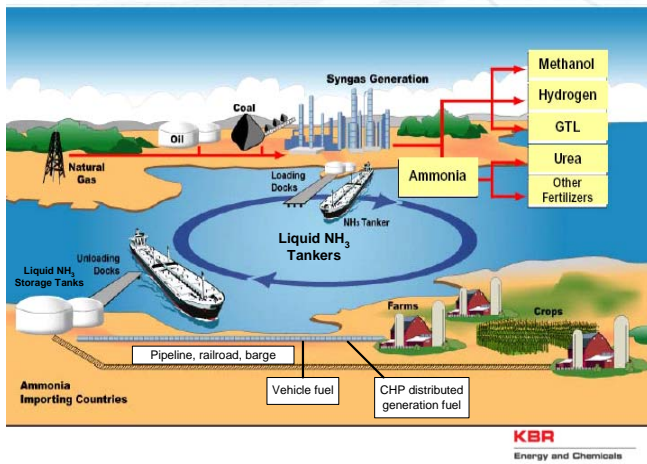


Fig. 5. Anhydrous Ammonia NH₃ Fuel Network. This paper assumes NH₃ production entirely from RE resources, with primarily terrestrial pipeline transmission. Globally, NH₃ is the second-largest volume industrial chemical.

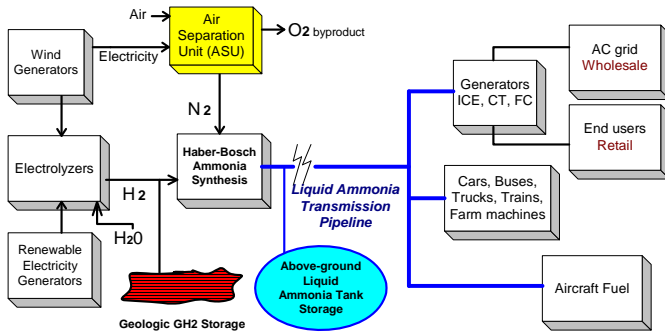


Fig. 6. NH₃ energy system: production from RE, with large-scale, low-cost energy storage and transmission for fuel distribution at distant markets.

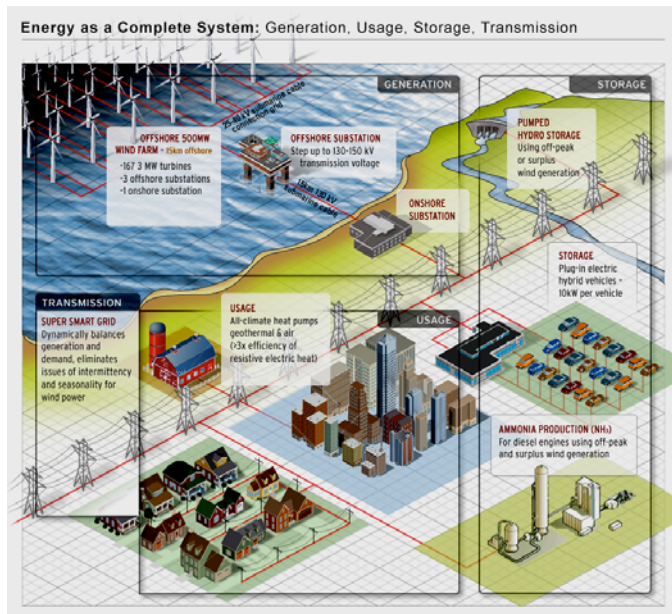
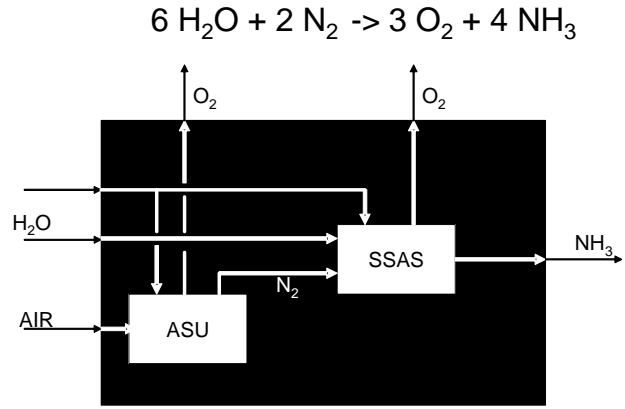


Fig. 7. Complete RE systems analysis must guide humanity’s investments in diverse, yet complementary, transmission, firming, and distribution strategies. Note Ammonia Production, for which inexpensive storage tanks are available. [11]



Energy consumption 7,000 – 8,000 kWh per ton NH₃

Fig. 8. Solid state ammonia synthesis (SSAS), an alternative to electrolysis plus Haber-Bosch synthesis, for NH₃ production from RE.



Fig. 9. Extant liquid NH₃ pipeline and storage terminal network, handling ~15 MMT per year, primarily for N-fertilizer, of which ~60% is imported.

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John H. Holbrook Dr. Holbrook is a materials scientist by training (University of Cincinnati, BS, and Stanford University, MS and PhD) and had a nearly 30-year career with Sandia National Laboratory Livermore, Battelle Columbus Labs, and the Pacific Northwest National Laboratory. Holbrook retired from PNNL in 2006, and has been devoting his efforts to help promote hydrogen technologies, in particular anhydrous ammonia as a zero-emission, sustainable hydrogen carrier for mobile and stationary applications. Holbrook is Executive Director of the Ammonia Fuel Network, an international group of technical and business representatives advancing ammonia as a direct fuel and hydrogen carrier. Holbrook has been working in the hydrogen energy field since the late 1970s, particularly in hydrogen storage and transport, and is very familiar with the "Hydrogen Economy" and how anhydrous ammonia can help overcome some hydrogen's technical challenges. Holbrook is a principal of NHThree LLC, formed to commercialize a green ammonia synthesis technology called Solid State Ammonia Synthesis (SSAS).